Renewable Hydrogen for the Pacific

Lecture 3: Hydrogen Safety and Economics

Hydrogen Safety and Economics

- This lecture will cover:
	- Hazards associated with gaseous and liquefied hydrogen
	- Safety protocols for hydrogen production, storage, and transportation
	- An introduction to hydrogen economics

Hydrogen Safety

Hydrogen Properties: Comparison

The Hindenburg Disaster

- The Hindenburg airship caught fire and was destroyed on May 6th 1937, causing 35 fatalities of the 97 on board
- The most accepted theory is that static electricity ignited both the canvas (painted in an incendiary mixture) and leaking hydrogen, eventually reaching the hydrogen stores
- Public confidence in airships (and hydrogen) was shattered

Other Incidents

- Many other hydrogen-related incidents have occurred:
	- \geq 1948: Hydrogen explosion at synthetic liquid fuels laboratory
	- \geq 2008: Fatal accident due to bacterial hydrogen production in atmospheric storage tank
	- \geq 2011: Hydrogen explosion and iron dust flash fires in powdered metals plant
	- ➢ 2011: Fukushima Daiichi nuclear disaster hydrogen explosions
	- ➢ 2020: Hydrogen tanker crash and explosion

Common Causes of Hydrogen-Related **Incidents**

- Equipment failure
- Human factors/errors
- Design errors, such as lack of leak detection, insufficient purging, incompatible materials etc.
- Insufficient maintenance
- Flaws in/failure to follow training including operating procedures
- Poor management of change
- Insufficient storage/monitoring protocol
- Flammable mixtures in confined space
- Collisions

Hydrogen Leakage

- Molecular hydrogen is the smallest and lightest of all gases
- It has a very high tendency to leak, and a fast escape rate
- Metals or alloys exposed to hydrogen can degrade or crack, causing hydrogen leakage
- This is known as hydrogen embrittlement or hydrogen attack

Hydrogen Leakage

- Odourants are added to natural gas to assist in detecting leaks
	- Natural gas for public gas supplies typically contains 5-10 mg of mercaptans, alkyl sulfides or cyclic sulfides per cubic meter of gas
- However, sulfur acts as a poison for the noble metal catalysts used in hydrogen fuel cells. Removal of the odorant would add significant expense
- Odorants also cause issues with hydrogen storage. For example:
	- Odorants will condense prior to condensation of hydrogen in cryogenic hydrogen storage
	- Odorants may strongly adsorb and block adsorption sites in metal hydrides and adsorbent-based storage

Hydrogen Leakage

- Alternative detection includes:
	- Hydrogen detection devices are costly, cumbersome, and require constant calibration
	- Devices can have:
		- \triangleright Detection sensitivity of +/- 0.25% by volume of H₂ in air
		- \triangleright Response time of <1 second at 1% H₂ in air
	- Non sulfur-based odorants, such as ammonia or ethyl isobutyrate. Fuel cell performance degradation is still an issue with these alternatives

Hydrogen Gas Detection Technologies

- Pellistor (or catalytic bead)
	- Use of a catalyst that causes flammable gas within the sensor to ignite at a much lower temperature than usual. Typically used as a general "catch-all" technology for flammable gas detection
- Electrochemical
	- Hydrogen is reacted with an electrolyte, producing a current, allows for much more sensitive hydrogen gas detection compared to pellistor sensors (0-1000 ppm)
- Semiconductor
	- Typically respond to a wide range of other gases and vapours.
- Thermal conductivity
	- Low sensitivity and selectivity render them poor for hydrogen detection applications
- Infrared
	- Unable to detect hydrogen since diatomic molecules like hydrogen don't absorb infrared radiation

Pellistor detector

Hydrogen Flammability

- Hydrogen leakage is an issue due to the extreme flammability of hydrogen
- Hydrogen has a very wide flammability range
	- From 4% to 74% in air, even more in atmosphere rich in oxygen or chlorine
- Hydrogen has a very low ignition energy
- Hydrogen burns with a pale blue flame, that is nearly invisible in daylight. Thermal and optical sensors should be used
- The risk of fire and explosion is therefore very high in some applications

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Reaction with Chlorine

• Hydrogen reacts spontaneously with chlorine:

 H_2 **+ Cl**₂ \rightarrow **2HCl**

- The reaction is slow in the absence of light but explosive when light or heat are present
- Hydrogen chloride is a colourless gas that forms hydrochloric acid upon contact with atmospheric humidity

Accidental Hydrogen Production

- Hydrogen may be accidentally produced through several pathways, resulting in documented industry accidents
- Via corrosion of steel:
	- \triangleright Steel is attacked by weak acids, releasing hydrogen

 $\text{Fe} + 2\text{H}^+ \rightarrow \text{Fe}_2^+ + \text{H}_2$

- \triangleright Steel is especially sensitive to pitting corrosion in the presence of aqueous solutions charged with chlorine, bromine, or hypochlorite ions
- Reactions of water or acids with metals
	- \triangleright Alkaline metals (Li, Na, K etc.) react rather violently with water and generate hydrogen

 2 Na + 2H₂O \rightarrow 2NaOH + H₂

- Formation of water gas
	- \triangleright Water gas (H₂ and CO), is formed when carbonaceous materials at very high temperatures (1000°C) come into contact with water

Other Hazards

- Gaseous Hydrogen
	- \triangleright No odour or taste, making leaks difficult to detect
	- \triangleright Non-toxic but can be an asphyxiant if it dilutes or displaces air
- Liquid Hydrogen
	- \triangleright Low temperature, causing damage to delicate tissue
	- \triangleright Loss of hydrogen to boil-off, drastically increasing pressure within the vessel
	- \triangleright Causes the condensation of other gases, e.g. causing solidified air to plug pipes and orifices and jam valves

Advantageous Properties of Hydrogen

- Hydrogen exhibits several safety-related advantages compared to conventional fuels:
	- \triangleright Hydrogen is non-toxic
	- \triangleright Combustion of hydrogen produces only water, compared to carbon monoxide released through incomplete combustion of carbon-based fuels
	- \triangleright The low density of hydrogen (14 times lighter than air and 57 times lighter than gasoline vapour) causes it to rapidly dissipate in air if leaked

Why is Hydrogen Safety Important?

- Hydrogen is intrinsically hazardous
- As hydrogen use becomes more widespread in industry and the community, management is critical to ensure safety during:
	- ➢ Production
	- ➢ Storage
	- \triangleright Handling and transport
	- \triangleright End use
- Therefore, safety rules, regulations, and standards are required to prevent dangerous incidents from occurring

A Typical Compressed Hydrogen Storage **Tank**

TPRD - Thermally Activated Pressure Relief Device Credit: Process Modeling Group, Nuclear Engineering Division. Argonne National Laboratory (ANL)

Existing Safety Controls for Compressed Hydrogen

- Type I:
	- \triangleright Composed of metal
	- \triangleright Cheap but low maximum pressures
- Type II:
	- \triangleright Metallic liner with a composite fiber and resin overwrap
	- \triangleright Improved mechanical strength but high cost
- Type III:
	- \triangleright Carbon fiber composite pressure vessel with a metal liner
	- \triangleright Improved mechanical strength but high cost
- Type IV:
	- \triangleright Carbon fiber composite pressure vessel with a polymer liner
	- \triangleright Reduced risk of hydrogen embrittlement at a higher cost

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Existing Safety Controls for Compressed Hydrogen

- Metals used are generally aluminium or steel
- Polymers used are generally high-density polyethylene or polyamide
- Carbon fibre is commonly used

A Type IV tank produced by Quantum **Technologies**

- Features:
	- \triangleright An impact-resistant foam dome
	- \triangleright An impact resistant outer shell, which is bulletproof and provides the tank with cut/abrasion resistance
	- \triangleright A carbon fibre reinforced plastic (CFRP) shell
	- \triangleright A polymeric liner
	- \triangleright Pressure and temperature sensors
	- ➢ Pressure relief device

Pressure Relief Devices

- PRDs are the main safety feature for compressed hydrogen storage
- A PRD protects against a failure of a storage vessel by releasing some or the entire tank content in the event of high temperatures, high pressures, or both
- Thermally-activated PRDs release hydrogen from a high-pressure storage container before its walls are weakened by high temperatures

Compressed Hydrogen Storage System

Indoor Storage - Safety Considerations

Safety considerations for indoor storage or use of bulk gaseous hydrogen include:

- \triangleright Buildings shall be constructed of non-combustible materials.
- \triangleright Hydrogen sensors shall be installed at ceiling level near ventilation exhaust.
- \triangleright Install automatic shutoff that activates if a leak or fire is detected in the facility that is being supplied with hydrogen.
- \triangleright Avoid ignition sources in storage areas.
- \triangleright Classified electrical equipment shall be in close proximity to storage systems.
- \triangleright Gaseous hydrogen system components shall be electrically bonded and grounded.

Outdoor Storage - Safety Considerations

- Hydrogen cylinders and storage tanks should be stored outside at a safe distance from structures, ventilation intakes, and vehicle routes
- Separation distance requirements based on quantity of hydrogen
- A bulk hydrogen compressed gas system has a capacity of more than 5,000 scf and consists of:
	- \triangleright storage containers
	- \triangleright pressure regulators
	- \triangleright pressure relief devices
	- ➢ compressors
	- \triangleright manifolds and piping

Other Safety Controls for Hydrogen

- Storage of hydrogen must take into consideration location and volume of hydrogen, with the preference to have the system outdoors to allow for ventilation if required
- Controls are further detailed in existing safety Standards and include:
	- \triangleright Material selection and design
	- \triangleright Administrative e.g., standard operating procedures, risk assessments, training, emergency procedures
	- Ignition source control e.g., electrical installation, explosion proof equipment, electrical grounding, lightning protection, prohibit welding etc.
	- **Ventilation**
	- ➢ Exclusion zones
	- \triangleright Hydrogen venting and flare system
	- \triangleright Labelling, barricades and access control
	- Instrumentation for monitoring and alarming e.g., hydrogen leak detection, fire detection
	- \triangleright Testing and auditing
	- ➢ Fire protection e.g., automatic/manual shutdown, deluge or sprinkler systems, etc.

Australian Standards for Hydrogen

- Need uniform and comprehensive legislation across all levels of Government
- Australian Standards managed by the ME-093 Hydrogen Technologies committee
- Adopted the ISO standards for hydrogen to assist with safe and regulated use of hydrogen within Australia
- Need to address the following key areas:
	- ➢ Safety
	- ➢ Environment
	- ➢ Trade
	- \triangleright Education

Australian Standards for Hydrogen

- Five working groups within the ME-093 Technical Committee
	- 1. Production, Handling and Storage
	- 2. Pipeline and Gas Distribution Networks
	- 3. End Use Applications
	- 4. Fuel Cell Applications
	- 5. Mobility Applications

Examples of Current Standards

- AS 16110.1:2020, Hydrogen generators using fuel processing technologies
- AS ISO 14687:2020, Hydrogen fuel quality Product specification
- AS 22734:2020, Hydrogen generators using water electrolysis Industrial, commercial, and residential applications
- SA TS 19883:2020, Safety of pressure swing adsorption systems for hydrogen separation and purification
- AS ISO 16111:2020, Transportable gas storage devices Hydrogen absorbed in reversible metal hydride
- AS ISO 19881:2020, Gaseous hydrogen Land vehicle fuel containers
- AS 19880:2020, Gaseous hydrogen Fuelling stations
- AS 26142:2020 Hydrogen detection apparatus stationary applications

Codes and Standards for FCEVs

GTR (harmonized with ISO and SAE J2978) **FMVSS** SAE J2615 - System Performance SAE J2572 - Fuel Consumption Measurement SAE J2574 - General Vehicle Safety SAE J2617 - Stack Performance SAE J2574 - Design for Recycling PEM stacks

Installation **NFPA 2 and Local Codes NEC ASME 31.12 CSA HGV 4.9 - Stations** ISO 19880-1

Compression & Storage

NFPA 2 and Local Codes

CSA HGV 4.8 - Compressors

ASME BPVC - Storage

Other Relevant Standards

- Hydrogen can be store in alternate chemicals (such as ammonia, methane, and methanol)
- Standards exist for these chemicals:
	- ➢ AS 1940:2017 The storage and handling of flammable and combustible liquids
	- ➢ AS/NZS 2022:2003 Anhydrous ammonia Storage and handling
	- ➢ AS/NZS 60079 Equipment for Explosive Atmospheres
	- ➢ See: <https://www.standards.org.au/>

Future Regulations and Challenges

- Regulators still need to utilise standards as law
- Further development of technical standards in each of the five focus areas
- Hydrogen technology is an evolving field, new methods of generation, application and storage are rapidly emerging
- Need to develop and maintain relevant standards which provide clear guidance in its safe use and to ensure its benefits are
- Committees must be proactive to match with rate of growth and allow fast-tracked application of hydrogen within Australia

End Goal: Hydrogen must be viable with the end-use sectors and yield benefits

End Goal: Economically H₂ needs to achieve certain cost barriers to become economically viable

*Hydrogen California PEM Electrolysis (incl CAPEX) \$/kg **Hydrogen California SMR w/o CCS (incl CAPEX) \$/kg Source: S&P Global Platts

H2 Industry

- \blacksquare E.g., for the H_2 industry a standard cost barrier is set by fossil-based hydrogen generation
- **Creating a race to US\$1.5 (or A\$2) per kg H²**

Reference: [Platts Hydrogen Price Wall](https://www.spglobal.com/commaodityinsights/PlattsContent/_assets/_files/en/specialreports/energy-transition/platts-hydrogen-price-wall/index.html)

Importance of A\$2/kg

At a cost value of <A\$2/kg, Hydrogen would become viable for large-scale industry offtake and export

Reference: [National Hydrogen Roadmap, CSIRO](https://www.csiro.au/en/work-with-us/services/consultancy-strategic-advice-services/csiro-futures/energy-and-resources/national-hydrogen-roadmap)

Additional Reading Material on H2 Costs across different sectors in Australia: [Advisian Australian Hydrogen Market Study](https://www.cefc.com.au/media/nhnhwlxu/australian-hydrogen-market-study.pdf)

The economics is not so

straightforward

It's like an iceberg – but hopefully, one that does not sink

the H² Ship

Reference: <https://www.irena.org/publications/2022/Jul/Global-Hydrogen-Trade-Outlook>

The Levelised Cost of Product: Represents the average revenue per unit of product that would have to be generated that would be required to recover the investment cost into constructing and operating the Power to X facility, an assumed financial life and duty cycle.

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Just like you pay a unit price for electricity.

Hydrogen users will pay a unit price per kg/MWh of H² that will cover the

producer's costs

Image Courtesy of US NREL: NREL [Video on LCOE](https://www.youtube.com/watch?app=desktop&v=F2DdCyW73VA&ab_channel=NRELLearning)

Benchmarking Offtake Cost Thresholds Predicting Future Hydrogen Costs

What Makes Up A Levelised Cost of Hydrogen?

Hydrogen production from project mass and energy balance

What Costs are Involved?

- ➢ **Stage 1: Cradle** Project envisioned, Prefeasibility makes sense and offtake agreement in place
- ➢ **Stage 2: H² Production and Distribution** Investment into development of facility/Operations kick off – supply chain established
- \triangleright **Stage 3: H₂ End Use** H₂ reaches end user and return on investment begins
- ➢ **Stage 4: End of Life** The project comes to an end and the facility is decommissioned with equipment and material salvaged for reuse.

It's all about the money!

How are the costs distributed ?

Capital Cost Assessment

Direct Cost

+ Indirect Cost

+ Contingencies

= Total Capital Costs

- Direct costs = material and labor involved in actual installation of complete facility (65-85% of fixed-capital investment)
	- A. Equipment + installation + instrumentation + piping + electrical + insulation + painting $(50-60\%$ of fixedcapital investment)
		- 1. Purchased equipment (15-40% of fixed-capital investment)
		- 2. Installation, including insulation and painting (25-55% of purchased-equipment cost)
		- 3. Instrumentation and controls, installed (8–50% of purchased-equipment cost)
		- 4. Piping, installed (10–80% of purchased-equipment cost)
		- 5. Electrical, installed (10–40% of purchased-equipment cost)
	- Buildings, process, and auxiliary (10-70% of purchased-equipment cost) **B.**
	- Service facilities and yard improvements (40-100% of purchased-equipment cost)
	- D. Land (1-2% of fixed-capital investment or 4-8% of purchased-equipment cost)
- Indirect $costs$ = expenses which are not directly involved with material and labor of actual installation of com-П. plete facility (15-35% of fixed-capital investment)
	- A. Engineering and supervision (5–30% of direct costs)
	- B. Legal expenses $(1-3\%$ of fixed-capital investment)
	- Construction expense and contractor's fee (10-20% of fixed-capital investment)
	- D. Contingency (5-15% of fixed-capital investment)
- **Fixed-capital investment** = direct costs + indirect costs III.
- Working capital (10–20% of total capital investment) IV.
- **Total capital investment** = fixed-capital investment $+$ working capital V.

Operating Cost Assessment

Feedstock Costs

- **+ Operation Costs**
- **+ Maintenance Costs**
- **+ Overheads**

= Total Operating Costs

- **Manufacturing cost** = direct production costs + fixed charges + plant overhead costs
	- A. Direct production costs (about 66% of total product cost)
		- 1. Raw materials (10-80% of total product cost)
		- 2. Operating labor (10–20% of total product cost)
		- 3. Direct supervisory and clerical labor (10–20% of operating labor)
		- 4. Utilities (10–20% of total product cost)
		- 5. Maintenance and repairs (2-10% of fixed-capital investment)
		- 6. Operating supplies (10-20% of maintenance and repair costs, or $0.5-1\%$ of fixed-capital investment)
		- 7. Laboratory charges (10–20% of operating labor)
		- 8. Patents and royalties (0–6% of total product cost)
	- B. Fixed charges (10–20% of total product cost)
		- 1. Depreciation (depends on method of calculation-see Chap. 7)
		- 2. Local taxes (1-4% of fixed-capital investment)
		- 3. Insurance $(0.4-1\% \text{ of fixed-capital investment})$
		- 4. Rent $(8-12\%$ of value of rented land and buildings)
		- 5. Financing (interest) (0-10% of total capital investment)
	- C. Plant overhead costs (50–70% of cost for operating labor, supervision, and maintenance; or $5-15\%$ of total product cost) include costs for the following: general plant upkeep and overhead, payroll overhead, packaging, medical services, safety and protection, restaurants, recreation, salvage, laboratories, and storage facilities
- II. General expenses = administrative costs + distribution and selling costs + research and development costs $(15-25\% \text{ of the total product cost})$
	- A. Administrative costs (about 20% of costs of operating labor, supervision, and maintenance; or 2–5% of total product cost) include costs for executive salaries, clerical wages, computer support, legal fees, office supplies, and communications
	- B. Distribution and marketing costs (2-20% of total product cost) include costs for sales offices, salespeople, shipping, and advertising
	- C. Research and development costs $(2-5\%$ of every sales dollar, or about 5% of total product cost)
- **III.** Total product cost[†] = manufacturing cost + general expenses

Distribution Costs

(Storage + Transport)

Cost of Hydrogen Delivery by Distribution Method

The cost varies based on the transport medium

Cash Flow Statement

Cash Flow Statement Functions

- **Tracking of Cash Flows**
- Important economic parameters (Profit, Revenue Statement, Breakeven, Net Present Value etc.)

End Goal: Prefeasibility Study

Pre-feasibility studies involve a design concept of the project is developed and a preliminary cost analysis is conducted.

- **Tools:**
	- Technical Analysis: Resource Mapping, Mass/Energy Balance
	- \checkmark Business Case: Conduct NPV, IRR etc = Economic Attractiveness
	- \checkmark Sensitivity Analysis: How flexible the economics are = Robustness of Business Case
	- \checkmark Risk Analysis: SWOT Analysis = Determine Opportunity Costs and Project Risks
	- \checkmark Environmental and Social Analysis: Will the Society and Environment be affected?

Further Reading:

[https://ens.dk/sites/ens.dk/files/Glob](https://ens.dk/sites/ens.dk/files/Globalcooperation/prefeasibility_study_guidelines_final.pdf) [alcooperation/prefeasibility_study_g](https://ens.dk/sites/ens.dk/files/Globalcooperation/prefeasibility_study_guidelines_final.pdf) [uidelines_final.pdf](https://ens.dk/sites/ens.dk/files/Globalcooperation/prefeasibility_study_guidelines_final.pdf)

End Goal: FEED Study

- **FIRM** Front End Engineering Design FEED
- **What is included in FEED:**
- ✓ Detailed Project Design and Cost Estimates based on quotes from vendors and EPC contractors
- \checkmark Strategies to procure equipment and construct the facility
- \checkmark Workflow and project plan

End Goal: Reaching a Final Investment Decision (aka FID)

How to Make an FID:

■ Conduct a FEED/Pre-Feasibility Study: Check if design and economics make sense.

If Economics and Design \Box = FID (+) ive – Go ahead with proposed project

If Economics and Design $\begin{bmatrix} 1 \end{bmatrix}$ = FID (-) ive – Back to the drawing board

Shell gives go-ahead to key renewable hydrogen plant in Holland

A 200 MW electrolyser is to be built on the Tweede Maasvlakte in the port of Rotterdam and will be operational in 2025

8 July 2022 12:20 GMT UPDATED 11 July 2022 18:13 GMT

By Nishant Ugal

Supermajor Shell has taken a final investment decision to build a 200-megawatt electrolyser for the Holland Hydrogen I hydrogen plant, in the Netherlands.

The company announced the go-ahead for the development on Wednesday, predicting it would be "Europe's largest renewable-hydrogen plant once operational in 2025".

"The 200 MW electrolyser will be constructed on the Tweede Maasvlakte in the port of Rotterdam and will produce up to 60,000 kilograms of renewable hydrogen per day," it said.

Shell noted that the renewable power for the electrolyser will come from the offshore wind farm Hollandse Kust (Noord), which is partly owned by the company.

Grey to green

End Goal: Reaching a Positive Final Investment Decision

What makes a Positive FID:

- <u>Prefeasibility Study</u>: Estimates show capital can be raised and return on investment is achievable
- FEED: Results show that the project is technically feasible, socially acceptable and environmentally safe with the project equipment and facility deliverable within available capital limits.

Challenges

- The cost of low impact H₂ is still significantly high (2 x 3 times higher than fossil fuels).
- Of the US\$320 billion worth of committed hydrogen projects only 10% have reached FID.

The Way Forward

- The cost of hydrogen production is decreasing as the cost of electrolyser systems and renewable energy pricing are undergoing a decrease
- There is growing support from governments and industry to incentives and bridge the cost gap to spearhead the development of a hydrogen economy.
- In light of these factors cost of H₂ is likely to reach parity with A\$2/kg target by 2030.

Motivation for Open-Source Modelling

- The infancy of the market there is a lack of comprehensive tools and transparency.
- Data drives the results the variables are subjective and will vary from context to context.
- Tools can assist in benchmarking the cost and performance parameters required to achieve project parity.
- Iterative platform to build on new and emerging technologies can be added

Open-Source Modelling

H² Modelling and Costing

Ammonia Modelling and Costing

Methanol Modelling and Costing

Hydrogen Export Costing

Impact

